STUDY P2X BY FRAUNHOFER IMWS AND FRAUNHOFER IGB BIOCAT

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Agenda

- Introduction Fraunhofer IMWS and IGB/CBP
- Study P2X : Green Hydrogen
- Study P2X : Green Ammonia



The Fraunhofer Gesellschaft at a glance



25 527 Staff 72 Institutes and

Research Facilities

2,3 Billion Euro **Budget**

Europe

around the world

Fraunhofer IMWS at a glance

- Director:
 - Prof. Ralf B. Wehrspohn
- Locations:
 - Halle (Saale)
 - Schkopau
 - Freiberg
 - Soest
 - Leuna (2019)

- Key Figures:
 - 284 Staff
 - 20,4 Mio. € Budget
 - 25,4 % direct industrial revenue
 - Quality Management ISO 9001-2017



Fraunhofer IMWS Halle



Fraunhofer IMWS Schkopau

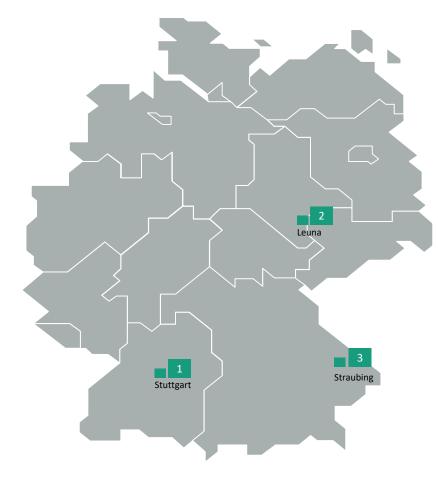


Fraunhofer IMWS Soest



Fraunhofer IGB

Director: Dr. Markus Wolperdinger





Thermal storage

Fraunhofer IGB Stuttgart (HQ)

Power-to-X Process engineering Wastewater treatment



Fraunhofer CBP Leuna Chem&Bio processes Power-to-X Upscaling of synthesis processes Biobased products



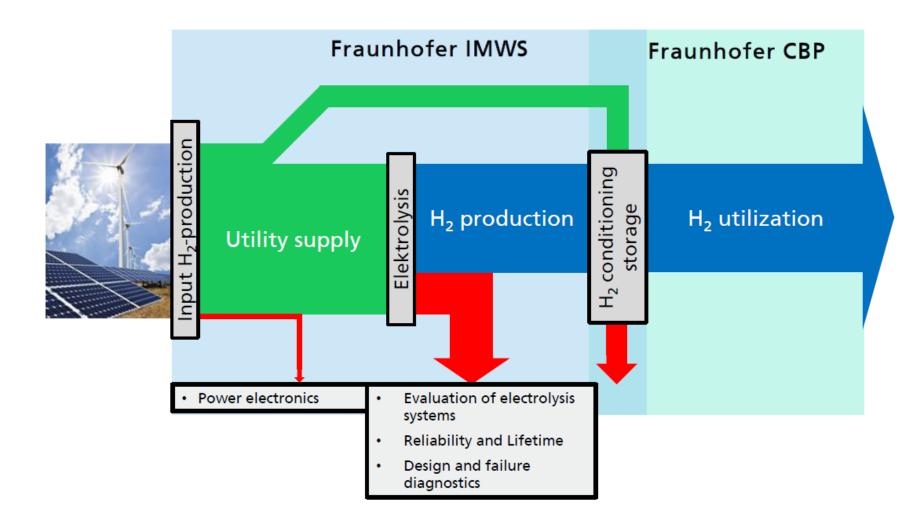
Fraunhofer IGB BioCat Straubing Power-to-X Chem&Bio processes Recovery of elements Biobased products

TRL 1-4

TRL 4-6



Fraunhofer IMWS – CBP – workshare

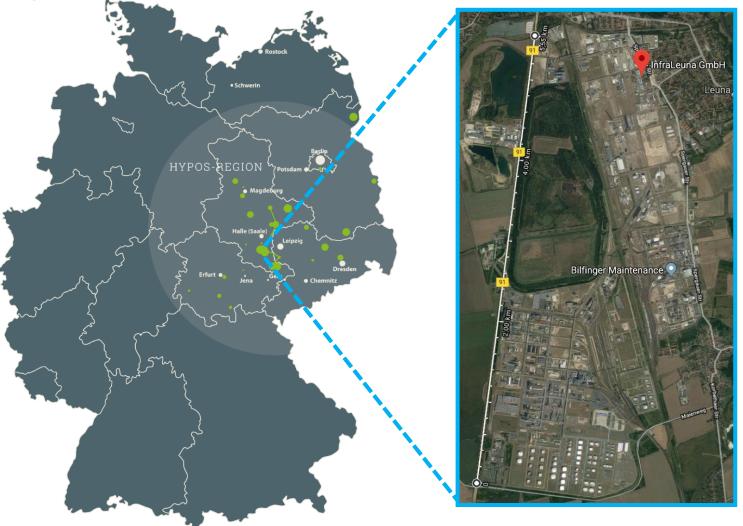




Fraunhofer IMWS Projects

Electrolysis research and test facility (ELP) Leuna

- Leuna Chemical Park operated by InfraLeuna
- Facts and figures:
 - 1,300 hectares
 - More than 10,000 employees
 - 600 km of pipeline network
 - 90 km of rail network





Seite 8

Electrolysis research and test facility (ELP) Leuna Project outline

- Planned by the two Fraunhofer Insitutes IMWS & CBP and co-financed by the State of Saxony-Anhalt
- Research infrastructure with labratories, office space and technical center
- Outside test area for containerized electrolysis systems, each space with a max. capacity of 5 MW
- Integrated into the Chemical side and connected to a 150 km long hydrogen/ pipeline and Remote Operation Center

 Visit Conter

 Visit Conter

 Visit Conter
- Opened for all electrolysis technologies (alkaline, PEM and high temperature SOEC)
- Fully operational in 2020





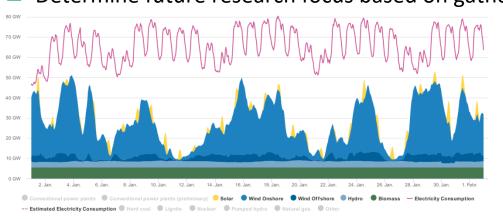
Kavernenspeicher





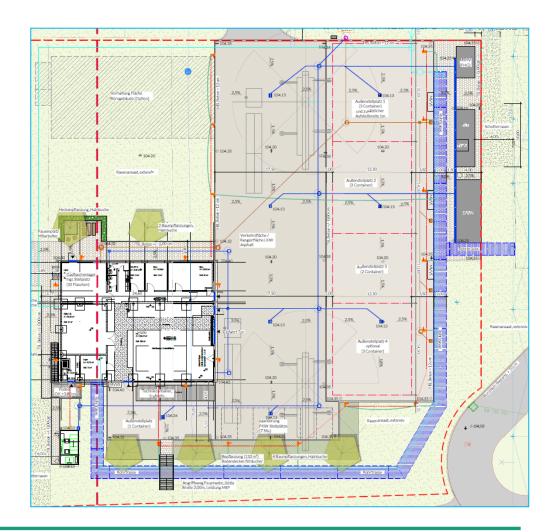
Electrolysis research and test facility (ELP) Leuna Scope

- Testing and evaluation of electrolysis systems up to 5 MW
- Demonstration of downstream processes for the use of H₂ (e.g. methanol synthesis)
- Creating energy and material balances in correlation with load profile
- Price of H₂ based on load profile



Determine future research focus based on gathered data



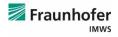


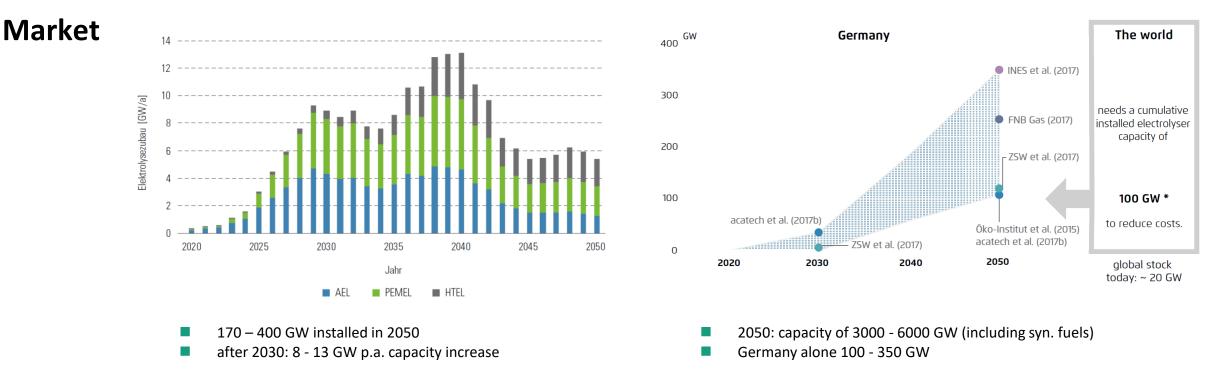




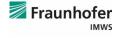
AGENDA STUDY P2X : GREEN HYDROGEN

- 1) Market development: PtX / Green Hydrogen
- 2) Technology comparison
- 3) Efficiency
- 4) Economy: CAPEX / OPEX analysis
- 5) combination with renewable energy (RE)
- 6) Requirement for Pilot Installation

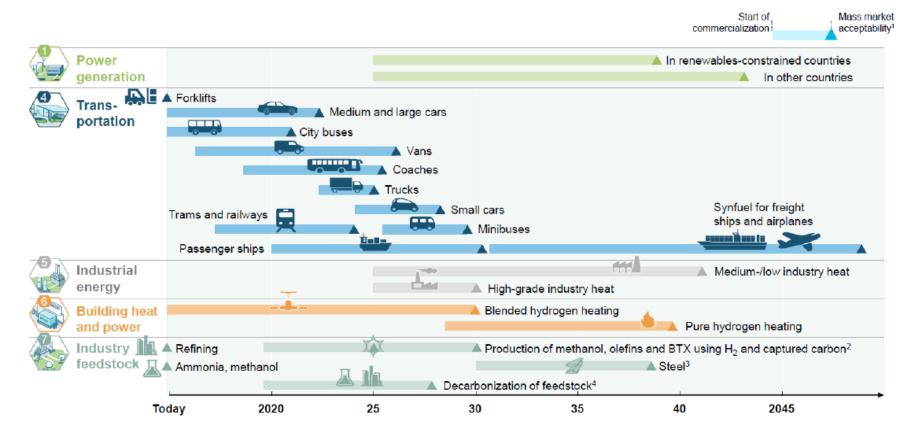




- PtX: multi GW technology in 2020-2030; significant variation of expected capacity
- Strongly dependent on applications (and regulatory framework in Germany)
- Hydrogen technologies in general and electrolysis are market ready
 - can be implemented into industrial applications

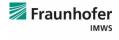


Applications

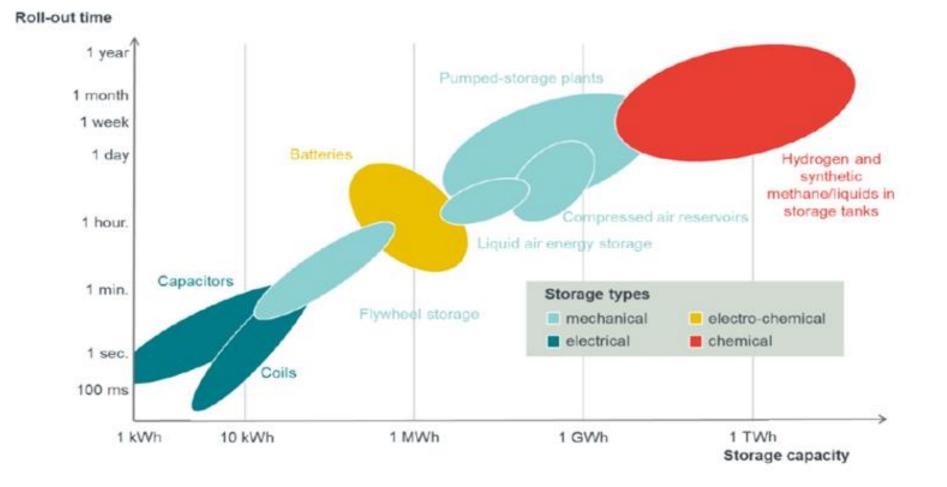


Applications in industry (Refining, Ammonia, ...) at initial phase

Long term energy storage (>1 year): No technologies except hydrogen available



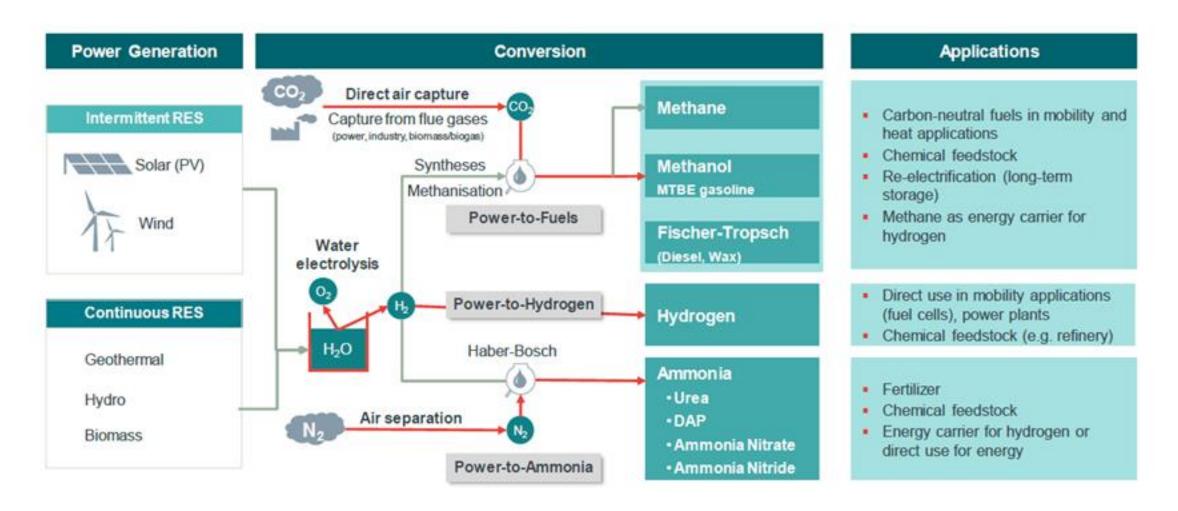
Technologies to store energy



Fraunhofer

Power-to-X:

Conversion of renewable power into various forms of chemical energy carriers





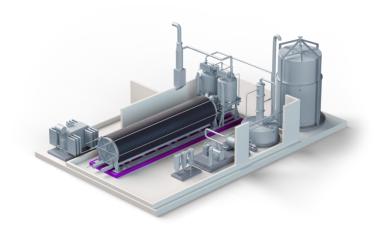
Electrolysis

Alkaline water electrolysers atmospheric

- Liquid electrolyte KOH
- Atmospheric pressure
- Proven technology in industrial scale



156 MW_{el} Hydrogen production for fertiliser plant completed in 1963 at the Assuan Dam in Egypt (source: ht-hydrotechnik)



NEL Hydrogen 485 Nm³/h Plans for 400 MW



ThyssenKrupp from chlor-alkaline electrolysis to water electrolysis



Electrolysis

Proton Exchange Membrane electrolyser

- Membrane as electrolyte
- High current desity
- Flexible from 0 200 %
- High pressure and atmospheric

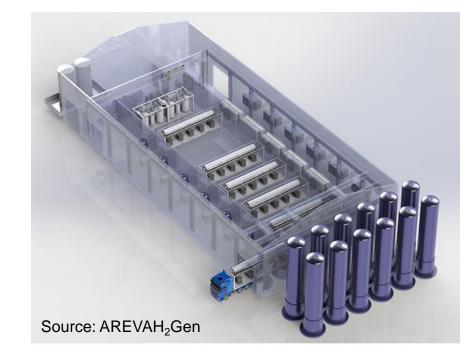




Source: Siemens Source: Giner Inc. Silyzer 300

Allagash 2 MW 400 Nm³/h

Source: Hydrogenics HyLIZER 600 3 MW 620 Nm³/h





Source: Proton OnSite



Electrolysis Solide Oxide electrolysis (SOEC)

- Solid Oxide as electrolyte
- High temperature process 750 1000 °C
- Steam as input media
- Reversible system possible



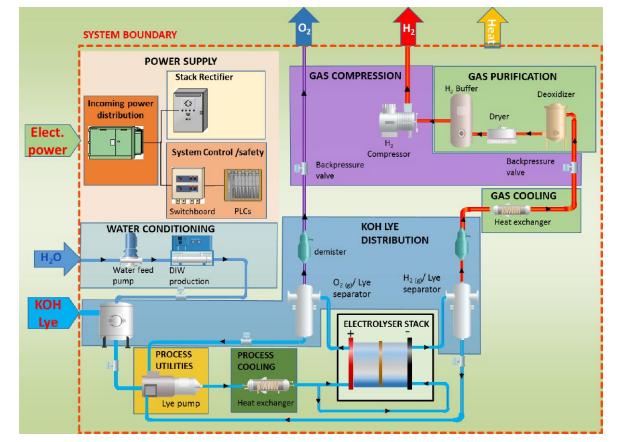
Source: Sunfire GmbH

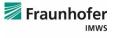


Technology

- electrolysis plant requires moderate complex system
- gaining experience of component interaction and system behavior essential for good plant management
 - especially for supply with RE
 - significant part of total cost stems from system components besides electrolyzer stack

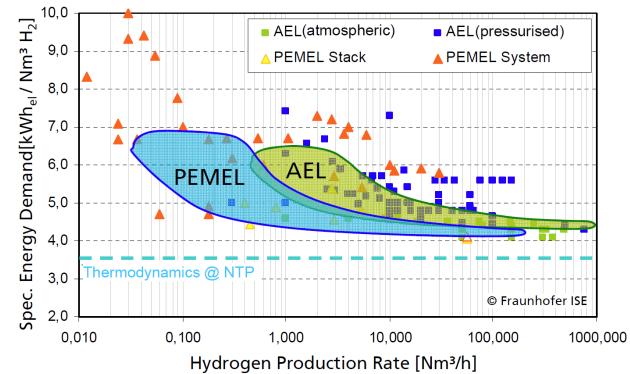
Example of alkaline electrolysis system





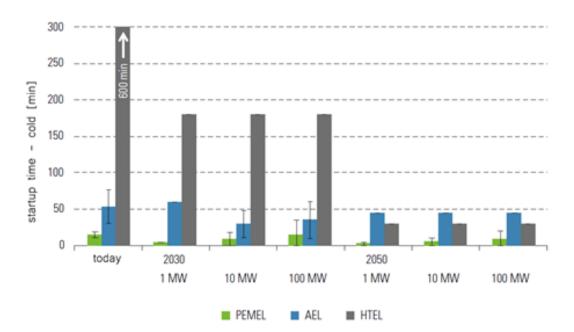
Efficiency

- Both technologies AEL and PEM at approx. same level of efficiency
- No significant future improvement of efficiency expected
 - technologies in pilot test, are also suitable for future production

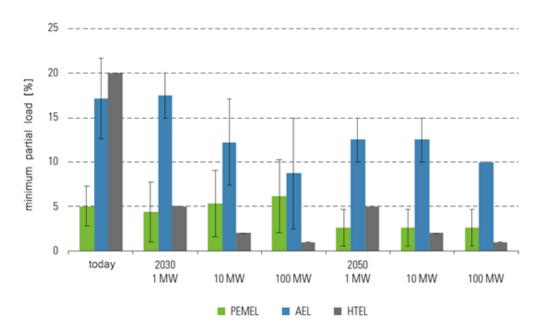




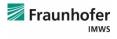
Parameters relevant for combination with fluctuating energy



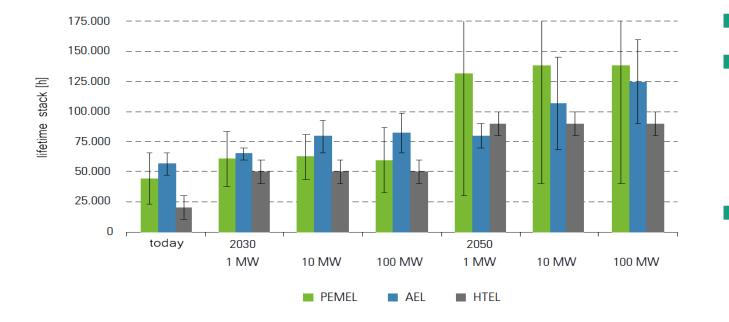
- time to start AEL and PEM from cold stack
- PEM < AEL < HTEL
- significant reduction for HTEL in future
- PEM is only technology with short start-up time



- capability of stack to run based on partial load
- today PEM lowest minimum partial load
- AEL & HTEL will lower current minimum values in the future



Reliability based of electrolysis system



currently AEL has highest lifetime

2030:

- increase in lifetime for all technologies
- nearly equal lifetimes for small scale systems in all technologies

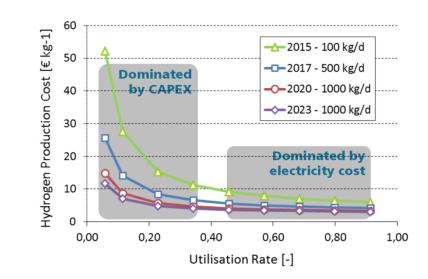
2050:

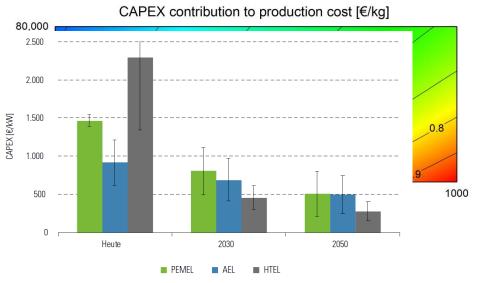
- AEL further increases lifetime for large scale systems
- PEM may become technology with highest reliability on all scales (high uncertainty)



Cost aspects - CAPEX

- CAPEX especially relevant for low utilization
- CAPEX today 900 1400 €/kW, expected minimum values of 500 €/kW (2020+, larger system)
- example calculation:
 - Energy for hydrogen production:
 - Investment cost for a EL-system:
 - lifetime of EL-system:
- CAPEX will decrease with further capacity build up / economy of scale





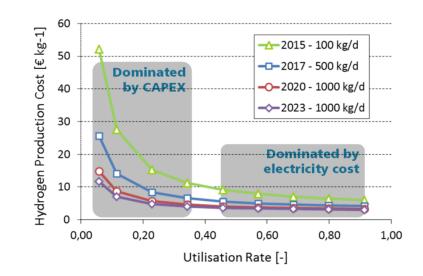


4.5 kWh/Nm³ 500 €/kW 60,000 h

→ 0.42 €/kg

Cost aspects - OPEX

- Main parameter: electricity cost
- Recent auction prices for RE:
 - Morocco: 4.8 ct/kWh (PV), 3 ct/kWh (wind)
 - Saudi-Arabia, Mexico: 1.8 ct/kWh
 - calculation for hydrogen price (assuming 4.5 kWh/m³ for energy need):



Power source	Electricity price [ct/kWh] [7]	Calculated OPEX [€/kg] Electricity
wind and PV in North Africa in 2020	5	2.5
PV in North Africa 2020	3.5	1.7
PV in North Africa 2050	2	1.0

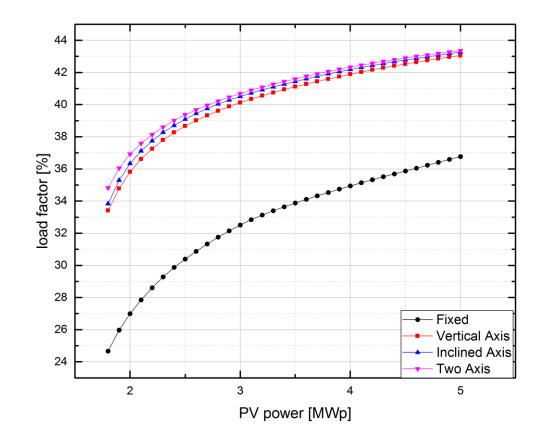
→ high load factor for the EL system is essential (PV alone will not suffice)

→ complete system setup has to be considered



Combination w. PV / renewable energy – a view on load factor

- economic operation requires high load factor
- simulation with PV data from [8] for Morocco
 (1.6 MW electrolysis plant)
- 1.6 MW PV (with tracking): load factor of ~34%
- combine PV and wind for more balanced power production throughout the day
 - wind power: prime energy source
 - PV plant serves as backup





Advantage of pilot installation

- invest in pilot will ensure:
 - right time for scale-up can be taken
 - technology with highest ROI (return on invest) can be taken
 - IP situation is well understood and secured
 - combination with RE is controlled
 - skill build up before major invest
- Future decisions for invest based on experience instead of assumptions.
- Experience in combination of hydrogen generation by electrolysis based on RE: define the best setup of the energy system
- future situation of Morocco regarding energy system can be taken into account





Opportunity for Morocco

Morocco could have an excellent position in future P2X industry, based on availability of RE



- At centre of PtX debate in Europe with strong PtX potential
- Energy partnerships with Europe foster political support
- Potential to lead technology development; may depend strongly on solid political facilitation

Morocco – the "hyped potential"

- Today: Strong RES potential identified by every study
- Short-term: Potential for larger-scale pilot projects
- Long-term: PtX development strong if politically facilitated



Snapshot of the world's strongest RES potentials

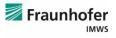


Thank you for your attention!



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Seite 27

AGENDA STUDY P2X: GREEN AMMONIA

- 1) Reviewing ammonia synthesis technologies
- 2) Catalysts, thermodynamics
- 3) Energy efficiency
- 4) Economy: CAPEX / OPEX analysis
- Intermittent operation :combination with renewable energy (RE)
- 6) Requirements for plant installation



Overview of ammonia synthesis technologies

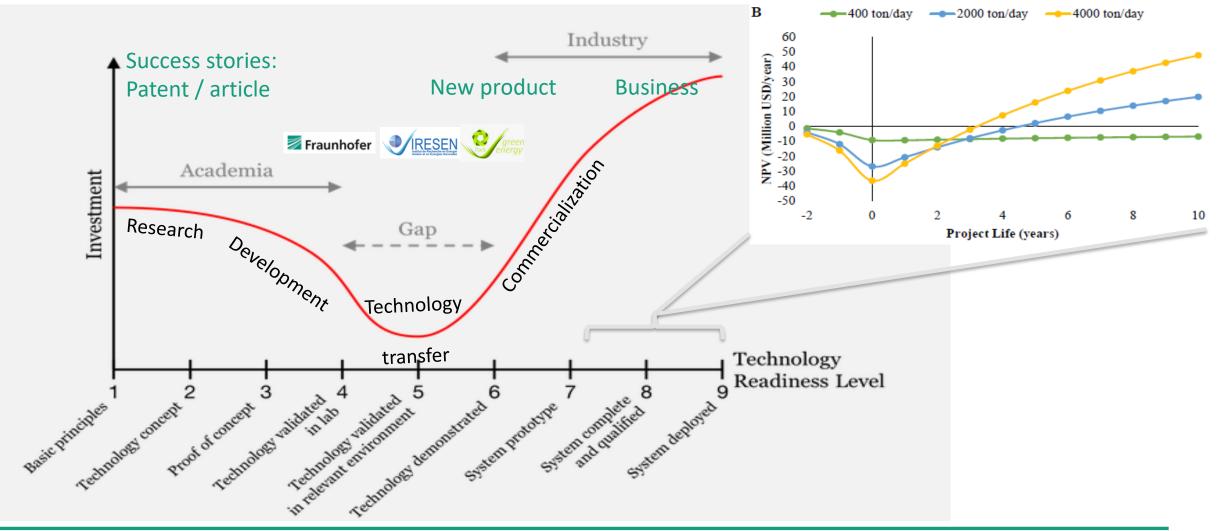
- Haber-Bosch process ٠
- direct electrochemical reduction of nitrogen to ammonia ۲
- photocatalytic reduction of nitrogen to ammonia and ۲
- plasma-enabled reduction of nitrogen to ammonia ٠

Reaction "drivers"	H ₂ needed from external source	No H ₂ needed from external source	Reaction "drivers"
Temperature, pressure catalyst	Haber-Bosch Synthesis	Direct electrochemical reduction of N ₂	Electrons, H ₂ O, electrocatalyst
Non-thermal plasma, catalyst, (temperature)	Plasma-enabled reduction	Photochemical reduction of N ₂	Photons, H ₂ O, photocatalyst



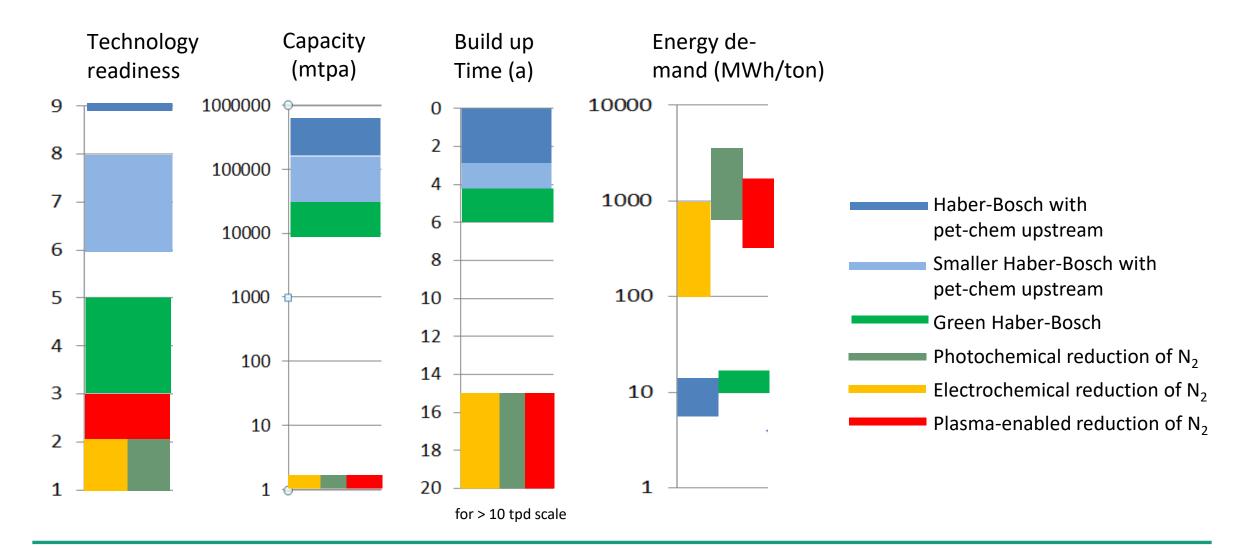
The long way from lab experiments to successful business case

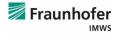
Technology readiness levels (TRL), investments and ROI





Ranking of the technologies





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Seite 31

Catalysts for Haber-Bosch process

Haldor-Topsoe

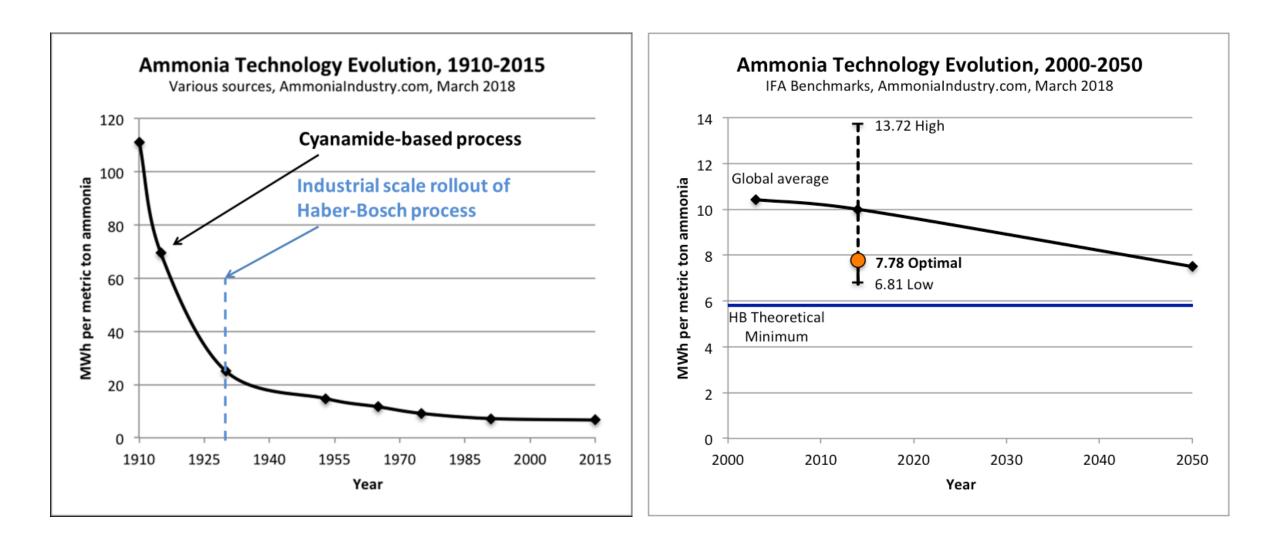
- KM-1: the magnetite based "industry benchmark" with long lifetime, over 1200 charges delivered
- KM111: more performant than KM1, better energy efficiency
- KM1R and KMR111: faster plant start-up than with KM1 and KM111

Clariant

- AmoMax10: increased activity compared to magnetite-based catalysts Johnson Matthey
- Katalco35: long lifetime, high activity
- Katalco74 superior activity in particular between 80 and 120 bar



Energy demand evolution of the Haber-Bosch process





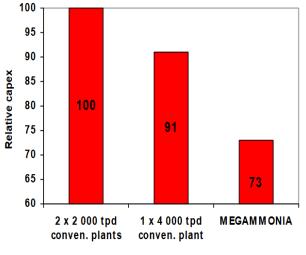
Company	Capacity (mtpa)	CAPEX (US\$)	CAPEX/t _{NH3} /d ay (\$/t/day)	Туре
Ammoni	715000	1,4 b	1958	Pet-Chem, greenfield
JV Yara&BASF	750000	600 m	800	H ₂ from other process
J.R. Simplot	Ca. 200000	350 m	1765	brownfield
Fortigen	Ca. 33000	75 m	2275	greenfield

Assuming 10 years payback time on the plant, the specific CAPEX is in the interval between 80 and 227 \$/ton NH3

Modularity:

CAPEX comparison

2x2000 vs 1x4000 tpd

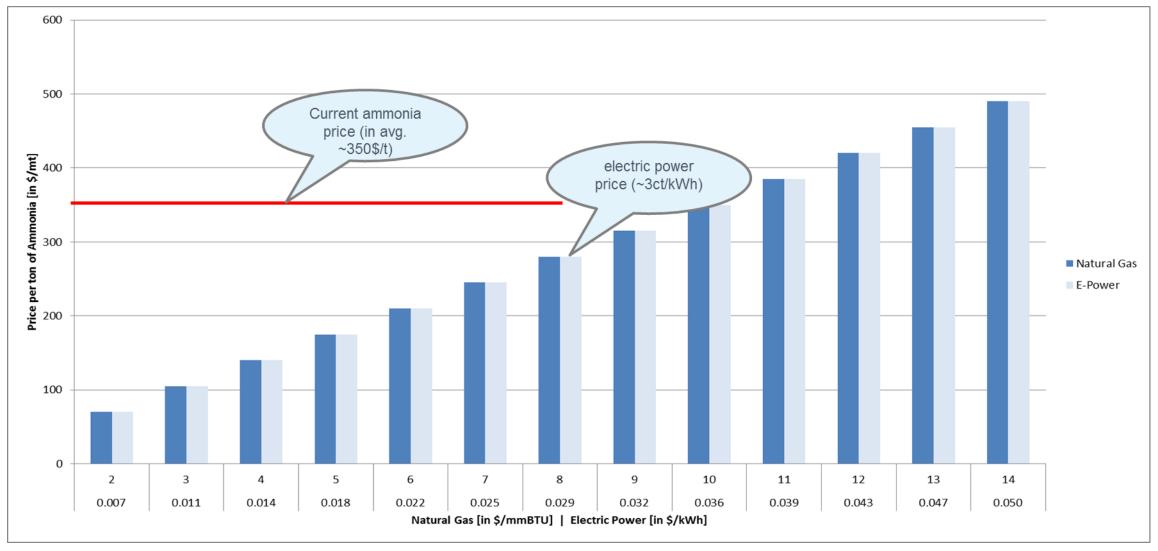


CAPEX Structure

MEGAMMONIA (Casale)

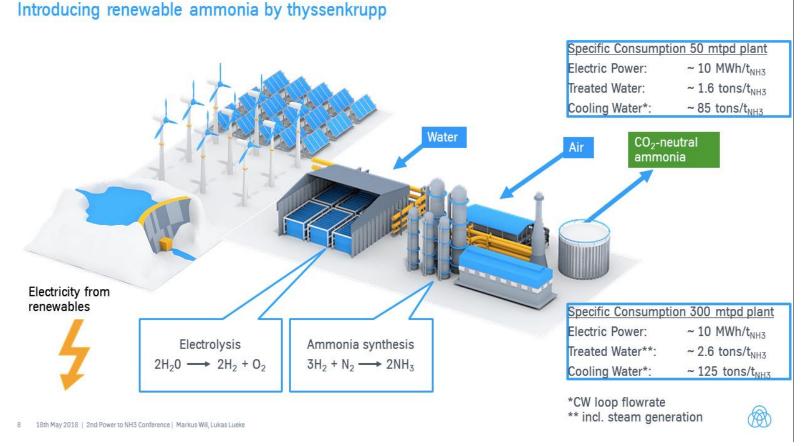
Process Plant	61 %
Utilities (including cooling tower)	15%
Tank farm (40 000 t NH3)	7 %
Air Separation Unit	<u>17 %</u>
TOTAL 1	00 %

OPEX estimation (energy price)





Green Ammonia plant by Thyssen-Krupp

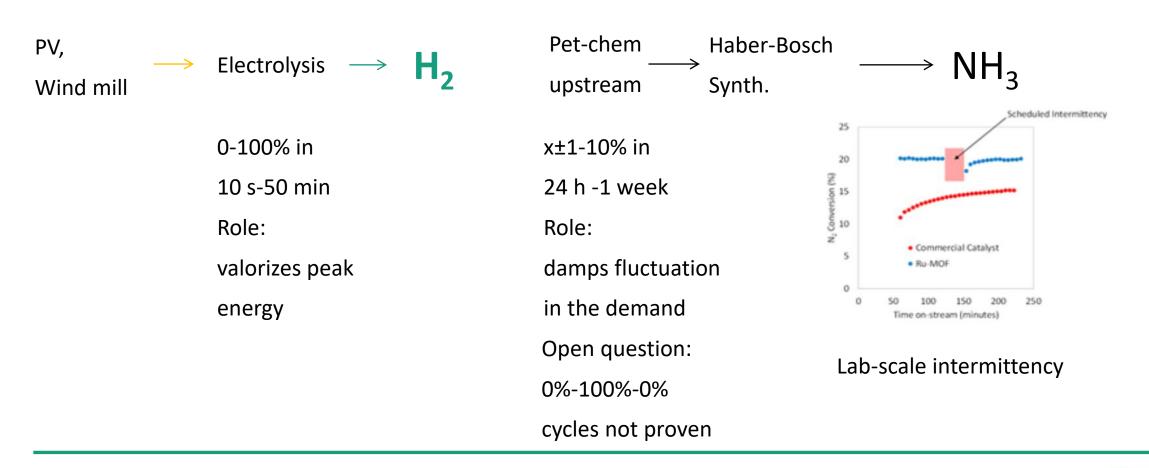


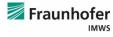
Location: Port Lincoln, AU CAPEX: 90 m \$ CAPEX/t/day: 4931 _{Aus}\$/t/d Target energy demand: 10 MWh/ton NH₃

"one of the first ever commercial plants to produce CO_2 -free 'green' ammonia from intermittent renewable resources."



Intermittent operation of lone standing technologies



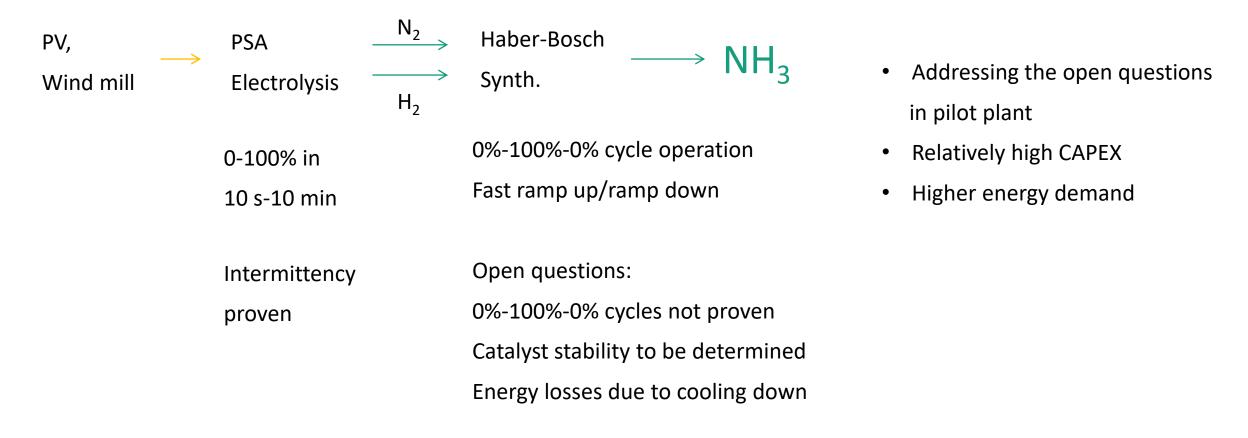


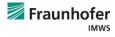
Seite 37

Addressing coupled intermittent operation on large scale

Scenario 1: Direct coupling of the electrolyzer and PSA with Haber-Bosch

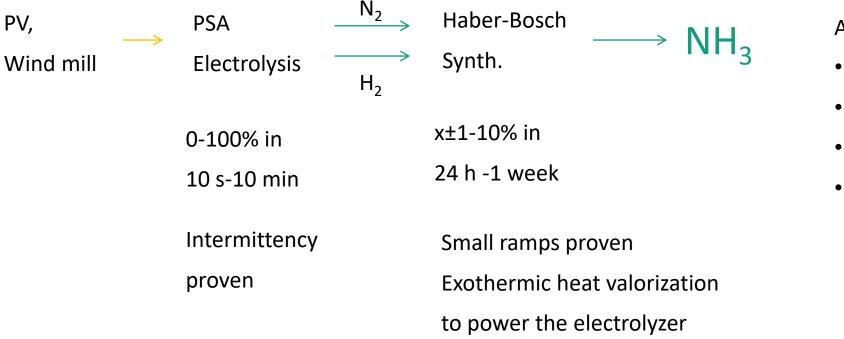
Condition: The Haber-Bosch reactor has to follow quasi real time the intermittency of the electrolyzer.





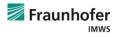
Addressing coupled intermittent operation on large scale

Scenario 2: Indirect coupling of the electrolyzer and PSA with Haber-Bosch Condition: The Haber-Bosch reactor may be operated with loads >0 %.



Advantages vs. Scenario 1

- Possible to build larger plant
- Significantly less R&D needed
- Better energy efficiency
- Maintaining >0% load factor of electrolyzer by feeding it with electricity from exothermal energy from the Haber-Bosch



Thank you for your attention!



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Seite 40



sources of information / literature

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[2] Frontier economics, from World energy council 2018 (INTERNATIONAL ASPECTS OF A POWER-TO-X ROADMAP, A report prepared for the World Energy Council Germany

[3] Hydrogen Council, McKinsey – Investor Day Presentation, 24.06.2018

[4] Tsotridis, G., & Pilenga, A. (2018). EU harmonised terminology for low temperature water electrolysis for energy storage applications.

[5] Smolinka, T., Water Electrolysis: Status and Potential for Development, Fraunhofer-institute for solar energy systems ISE, Water Electrolysis Day Brussels (BE), April 03, 2014

[6] Cost break down and cost reduction strategies for PEM water electrolysis systems, Presentation held at 6th European PEFC & Electolyser Forum, Lucern, Switzerland, July 5, 2017, Author(s): Smolinka, T.; Wiebe, N.; Thomassen, M.

[7] Study by AGORA Germany Agora Verkehrswende, Agora Energiewende and Frontier Economics (2018): The Future Cost of Electricity-Based Synthetic Fuels., <u>https://www.agora-energiewende.de/</u>

[8] <u>http://re.jrc.ec.europa.eu/PVg_tools/en/tools.html#PVP</u>

